

One of the most familiar relationships in chemistry is the ideal gas equation of state

$$PV = nRT$$

Sometimes written as:

$$P\bar{V} = RT$$

$$\bar{V} = ??$$

Gases that obey this equation behave *ideally*.

The ideal gas equation of state neglects:

1. The molecular size of gases.
2. Intermolecular interactions of gases.

Under what conditions is this neglect legitimate?



Extensive Variable: Depends on the size of the system (e.g., V, m, E)

mass ↘ Energy ↙

Intensive Variables: Doesn't depend on the size of the system (e.g., T, P, ρ)

Density ↗

What about *molar volume*?

Operational Definition of Temperature (unit of kelvin, K):

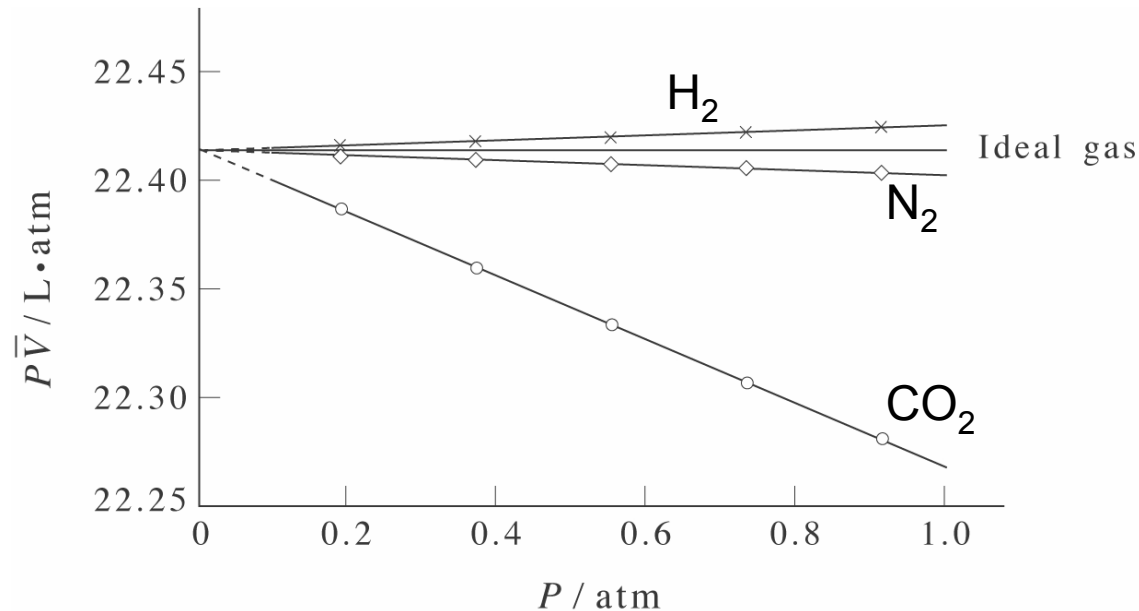
$$T = \lim_{P \rightarrow 0} \frac{P\bar{V}}{R}$$

$$t/^{\circ}\text{C} = T / \text{K} - 273.15$$



Gases are Rarely Ideal! I

GAS-3



At low enough pressures, *all* gases behave ideally.

$$P\bar{V}(273.15) = 22.414 \text{ L}\cdot\text{atm}\cdot\text{mol}^{-1}$$

$$R = \frac{P\bar{V}}{T} = 0.082058 \text{ L}\cdot\text{atm}\cdot\text{mol}^{-1}\cdot\text{K}^{-1} = 8.314 \text{ J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$$

(see Table 16.2)

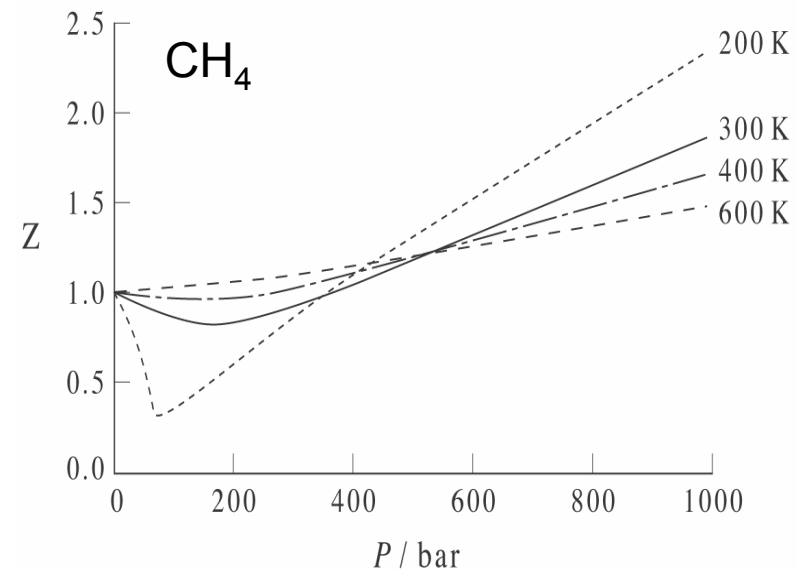
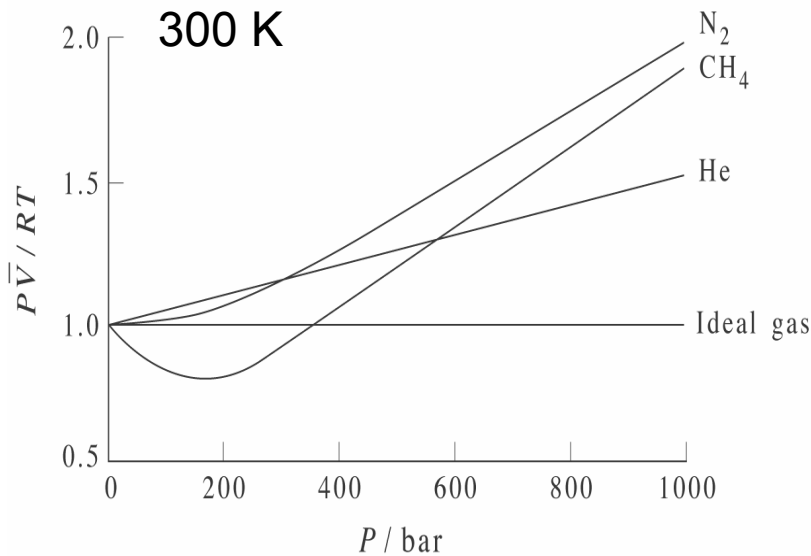


Gases are Rarely Ideal! II

GAS-4

$$Z = \frac{P\bar{V}}{RT}$$

Compressibility ← Units?
← Ideal Gas?



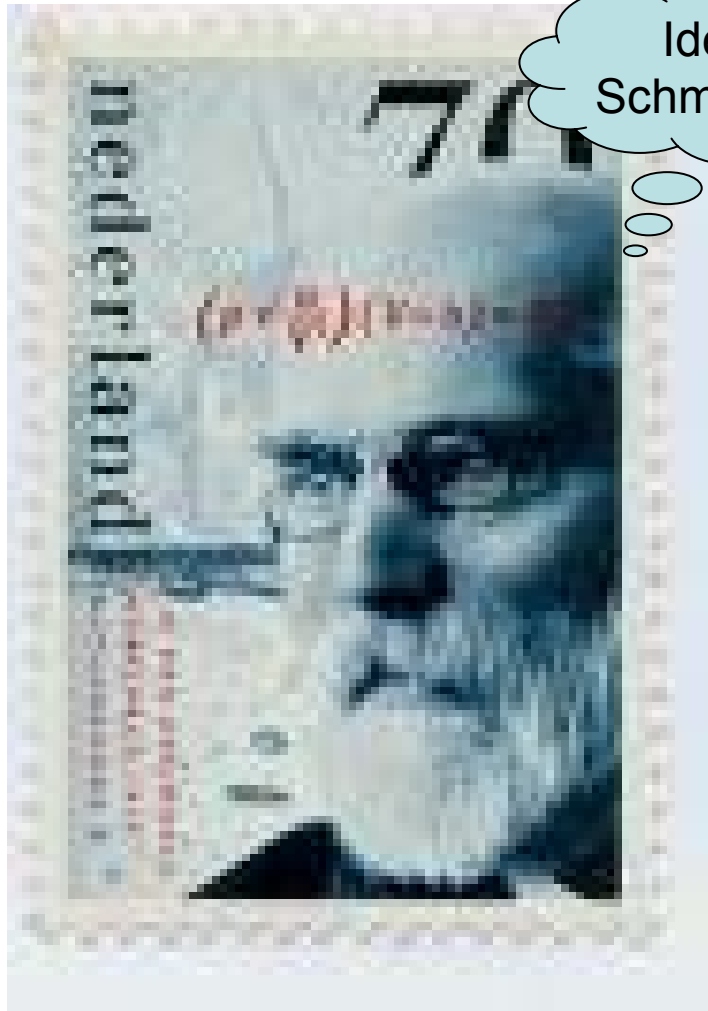
Low Temperature: Attractive forces

$$\bar{V}_{real} < \bar{V}_{ideal}$$

High Temperature: Repulsive forces

$$\bar{V}_{real} > \bar{V}_{ideal}$$





Ideal
Schmideal!

$$\left(P + \frac{a}{\bar{V}^2} \right) (\bar{V} - b) = RT$$

Van der Waals *Equation of State**

a and b are constants that depend on the specific gas in question:

a ~ intermolecular interaction strength

b ~ molecular size

	a (dm ⁶ ·bar·mol ⁻²)	b (dm ³ ·mol ⁻¹)
Helium	0.035	0.024
Ammonia	4.304	0.037

*This (and other equations of state) are cubic equations in terms of volume (this will become important!).



$$\left(P + \frac{a}{\bar{V}^2} \right) (\bar{V} - b) = RT$$

van der Waals

$$P = \frac{RT}{\bar{V} - B} - \frac{A}{T^{1/2} \bar{V} (\bar{V} + B)}$$

Redlich-Kwong

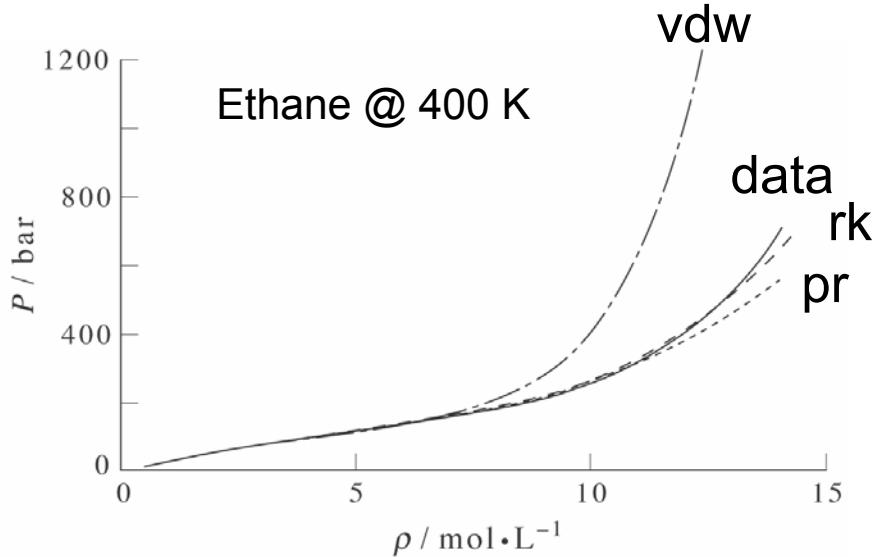
$$P = \frac{RT}{\bar{V} - \beta} - \frac{\alpha}{\bar{V} (\bar{V} + \beta) + \beta (\bar{V} - \beta)}$$

Peng-Robinson



vdw, rk, pr EOS

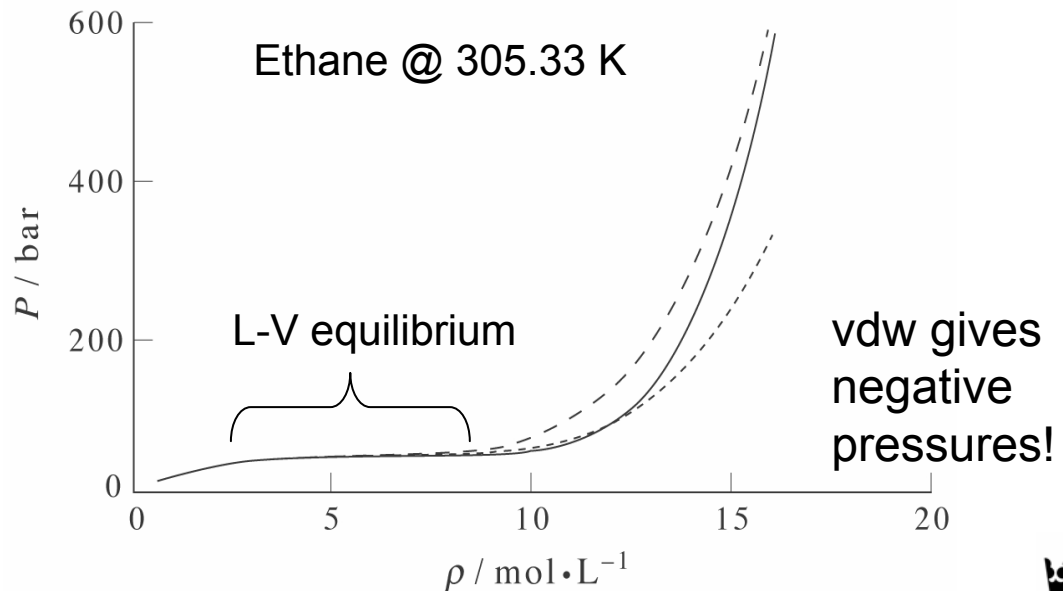
GAS-7

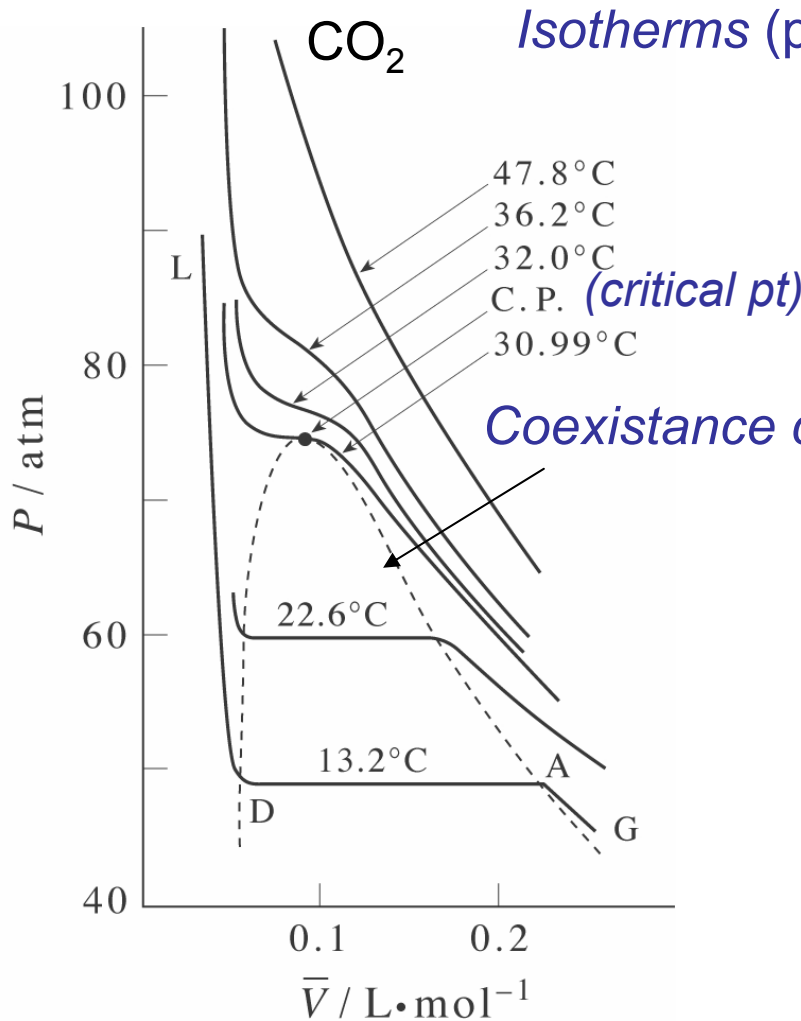


$$\bar{V}^{-1} = \rho \quad \text{Units?}$$

What would ideal gas law predict for such a plot?

These EOS describe gas properties well – and are nearly quantitative when the gas liquefies!





Isotherms (plots of P vs V at constant T)

Cubic EOS describe both the liquid and gaseous regions

The temperature above which a gas can not be liquefied is called the critical temperature (T_c).

At $T < T_c$, there are horizontal regions (gas and liquid co-exist).

G to A to D to L (@ 13.2 °C)

a

i

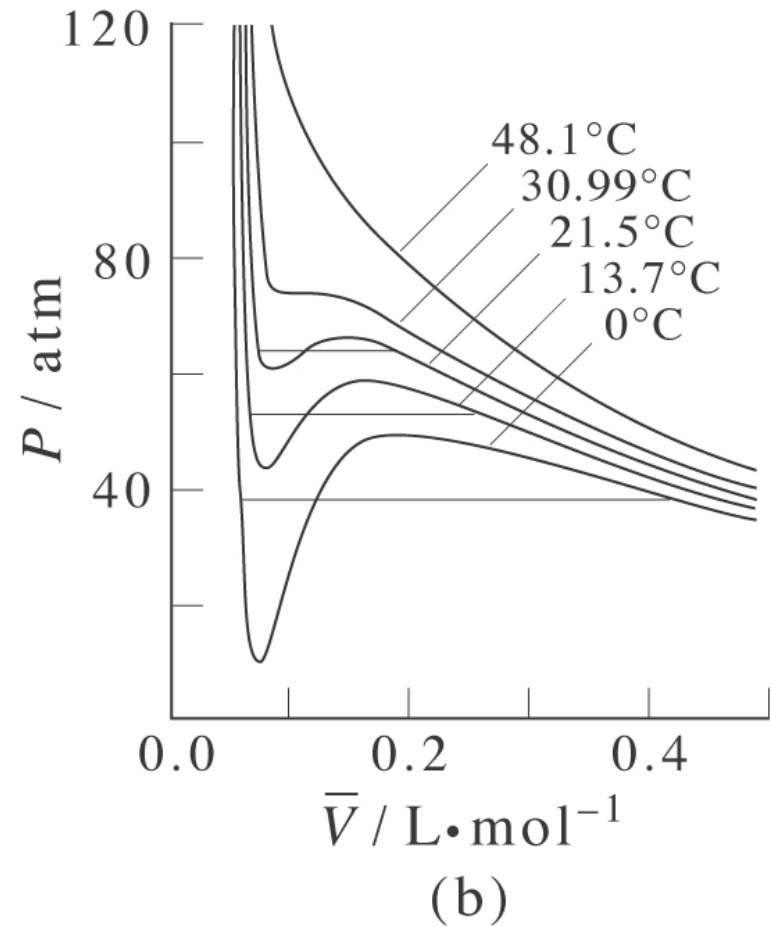
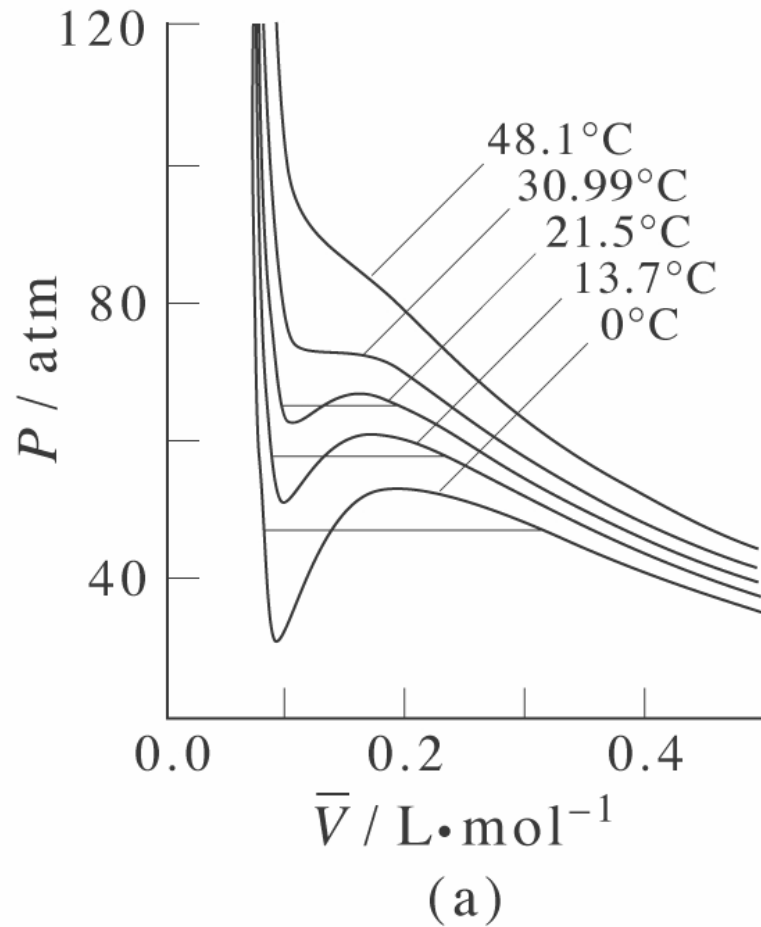
s

q



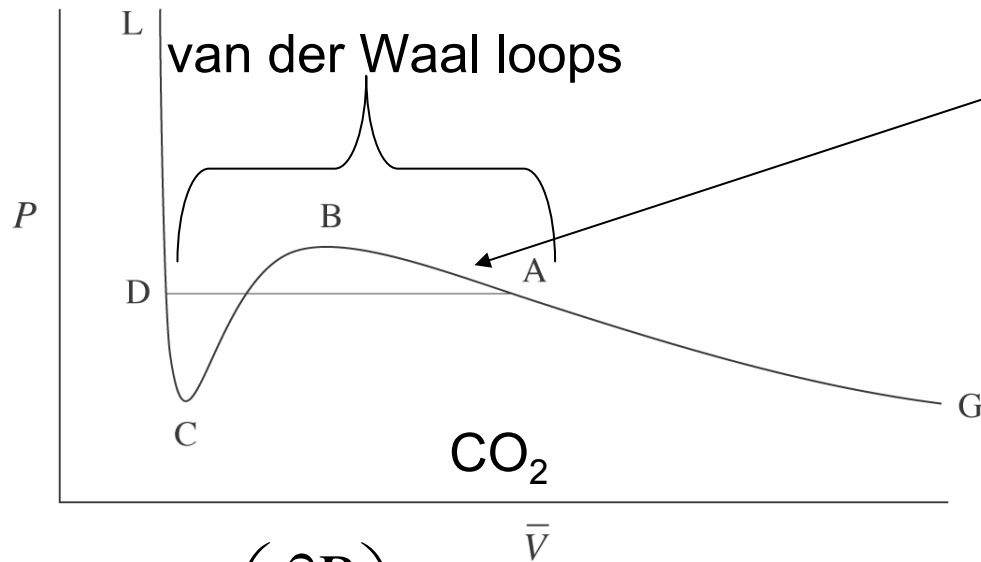
How do cubic EOS do for CO₂?

GAS-9



Not too bad...





Line DA is drawn such that areas of the loop both above and below DA are equal = Maxwell equal-area construction

What is sign of $\left(\frac{\partial P}{\partial \bar{V}}\right)_T$ from B to C? Is this realistic?

Three values of volume for a given pressure at $T < T_c$.

Remember: VDW EOS can be written as a cubic equation in molar volume!

$$\bar{V}^3 - \left(b + \frac{RT}{P}\right)\bar{V}^2 + \frac{a}{P}\bar{V} - \frac{ab}{P} = 0 \quad \text{Three roots!}$$



Critical Point in VDW P-V Isotherms GAS-11

$$\bar{V}^3 - \left(b + \frac{RT}{P} \right) \bar{V}^2 + \frac{a}{P} \bar{V} - \frac{ab}{P} = 0$$

At $T > T_c$ only one real root.
At $T < T_c$ three real roots.
At $T = T_c$ all three roots merge.

At $T = T_c$...

$$\bar{V} - \bar{V}_c = 0 \quad \text{or} \quad (\bar{V} - \bar{V}_c)^3 = 0$$

$$\bar{V}^3 - 3\bar{V}_c \bar{V}^2 + 3\bar{V}_c^2 \bar{V} - \bar{V}_c^3 = 0$$

Compare to VDW EOS and do some algebra...

$$\bar{V}_c = 3b \quad P_c = \frac{a}{27b^2} \quad T_c = \frac{8a}{27bR}$$



Critical Point in VDW P-V Isotherms GAS-12

TABLE 2.5 (Table 16.5)

The experimental critical constants of various substances.

$$\frac{P_c V_c}{RT_c} = \frac{1}{R} \left(\frac{a}{27b^2} \right) (3b) \left(\frac{27bR}{8a} \right) = ??$$

Species	T_c/K	P_c/bar	P_c/atm	$\bar{V}_c/\text{L}\cdot\text{mol}^{-1}$	$P_c \bar{V}_c / RT_c$
Helium	5.1950	2.2750	2.2452	0.05780	0.30443
Neon	44.415	26.555	26.208	0.04170	0.29986
Argon	150.95	49.288	48.643	0.07530	0.29571
Krypton	210.55	56.618	55.878	0.09220	0.29819
Hydrogen	32.938	12.838	12.670	0.06500	0.30470
Nitrogen	126.20	34.000	33.555	0.09010	0.29195
Oxygen	154.58	50.427	50.768	0.07640	0.29975
Carbon monoxide	132.85	34.935	34.478	0.09310	0.29445
Chlorine	416.9	79.91	78.87	0.1237	0.28517
Carbon dioxide	304.14	73.843	72.877	0.09400	0.27443

$$\frac{P_c \bar{V}_c}{RT_c} =$$

An example of the *Law of Corresponding States*



Law of Corresponding States

GAS-13

In practice, the experimental values for the critical temperature and pressure are used to get a and b .

$$a = \frac{27(RT_c)^2}{64P_c} \qquad b = \frac{RT_c}{8P_c}$$

VDW equation with a and b substituted with above equations:

$$\left(P + \frac{3P_c \bar{V}_c^2}{\bar{V}^2} \right) \left(\bar{V} - \frac{1}{3} \bar{V}_c \right) = RT$$

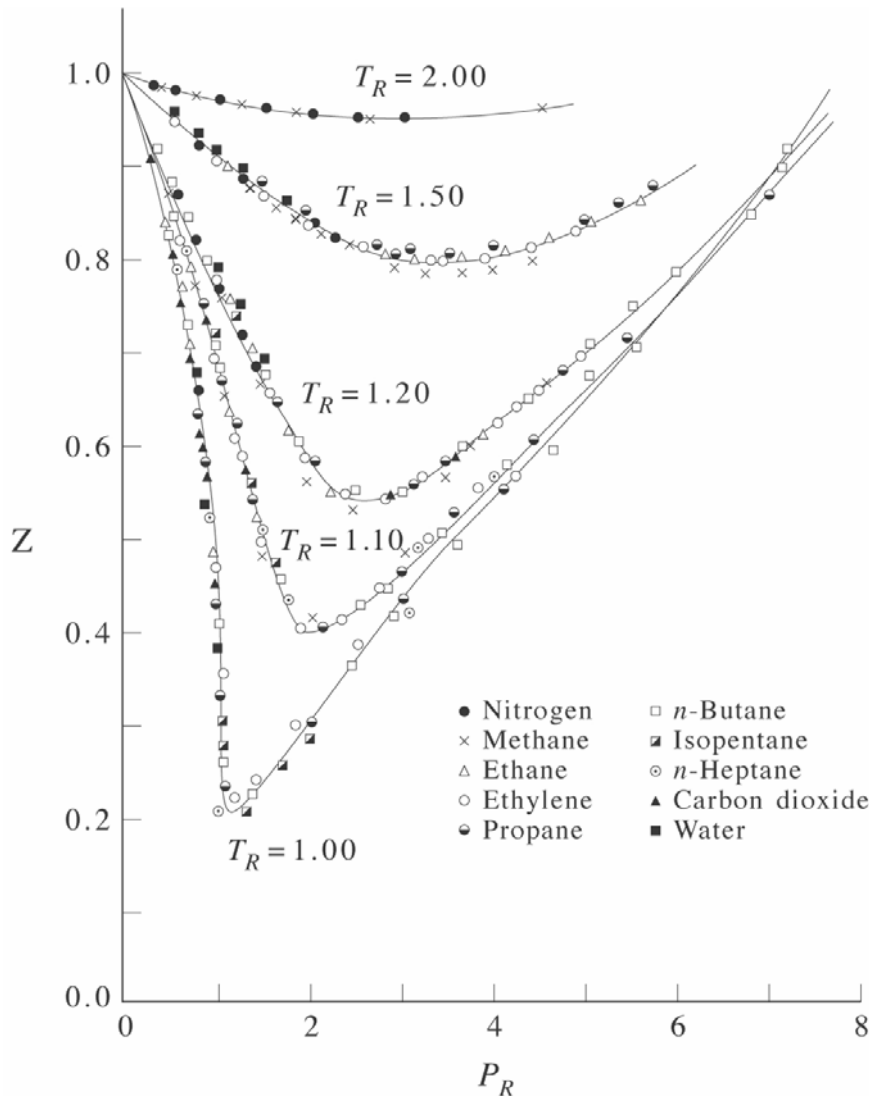
Let... $\bar{V}_R = \frac{\bar{V}}{\bar{V}_c}$, $T_R = \frac{T}{T_c}$, and $P_R = \frac{P}{P_c}$ to get:

$$\left(P_R + \frac{3}{\bar{V}_R^2} \right) \left(\bar{V}_R - \frac{1}{3} \right) = \frac{8}{3} T_R$$

Universal
equation for
all gases!

Law of Corresponding States The properties of all gases are the same if we compare them under the same conditions relative to their critical point.





The compressibility factor also obeys the LOCS. So Z has the same functional form for *all* gases at the corresponding conditions.

$$Z = \frac{P\bar{V}}{RT}$$

A gas “knows” its critical temperature, and is therefore “aware” of its temperature *relative* to its critical temperature ($T_R = T/T_c$).



Express the compressibility as an (infinite) series of terms to get an exact expression (more of a statistical model).

$$Z = \frac{P\bar{V}}{RT} = 1 + \frac{B_{2V}(T)}{\bar{V}} + \frac{B_{3V}(T)}{\bar{V}^2} + \frac{B_{4V}(T)}{\bar{V}^3} \dots$$

$$Z = \frac{P\bar{V}}{RT} = 1 + B_{2P}(T)P + B_{3P}(T)P^2 + B_{4P}(T)P^3 + \dots$$

B_{nV} are virial coefficient (e.g., B_{2V} is the second virial coefficient)

As the molar volume becomes large or the pressure becomes small...

$$Z = ??$$



2nd Virial Coefficient

The second virial coefficient is the first deviation from ideality (as a result of *intermolecular interactions*) as the pressure is increased (or molar volume is decreased).

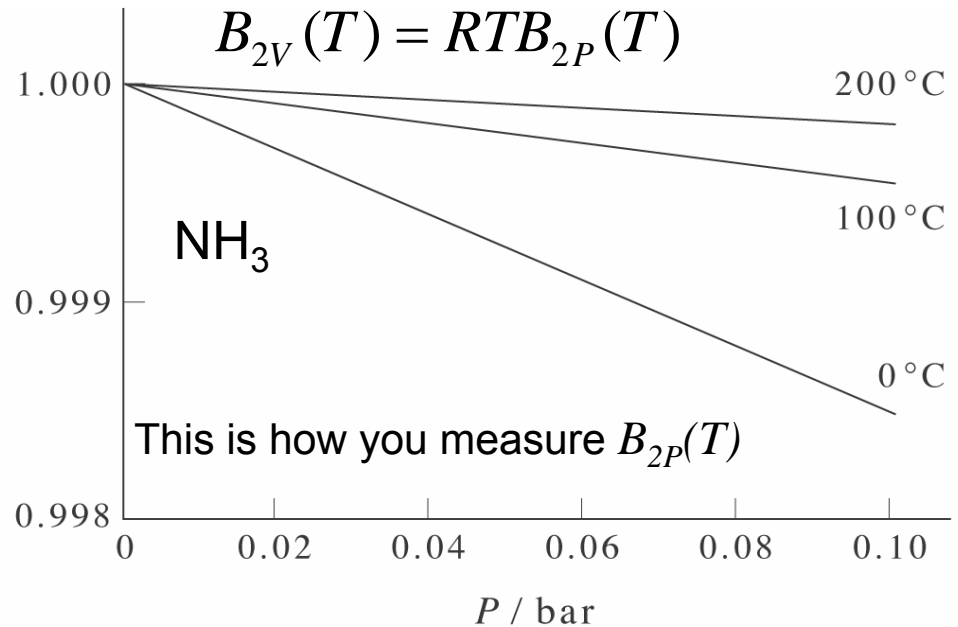


TABLE 2.6

The contribution of the first few terms in the virial expansion of Z , Equation 2.22, for argon at 25°C.

P/bar	$Z = P\bar{V}/RT$
	$1 + \frac{B_{2V}(T)}{\bar{V}} + \frac{B_{3V}(T)}{\bar{V}^2} + \text{remaining terms}$
1	$1 - 0.00064 + 0.00000 + (+0.00000)$
10	$1 - 0.00648 + 0.00020 + (-0.00007)$
100	$1 - 0.06754 + 0.02127 + (-0.00036)$
1000	$1 - 0.38404 + 0.08788 + (+0.37232)$

For ammonia...

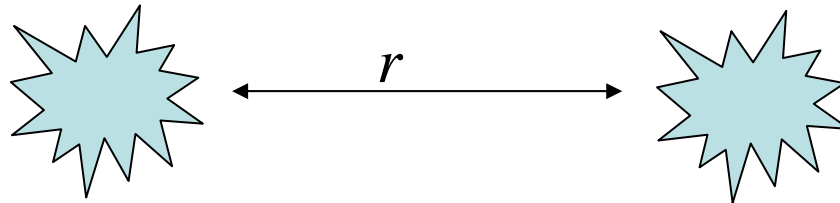
$$B_{2V}(0\text{ °C}) = -0.345 \text{ dm}^3 \cdot \text{mol}^{-1}$$

$$B_{2V}(100\text{ °C}) = -0.142 \text{ dm}^3 \cdot \text{mol}^{-1}$$

$$B_{2V}(200\text{ °C}) = -0.075 \text{ dm}^3 \cdot \text{mol}^{-1}$$



The virial expansions can be used to derive exact relationships between the virial coefficients and intermolecular interactions.



Consider 2 molecules and assume that their interaction depends only on how close they are to one another (r), the B_{2V} can be expressed as:

$$B_{2V}(T) = -2\pi N_A \int_0^{\infty} \left[e^{\frac{-u(r)}{k_B T}} - 1 \right] r^2 dr$$

If $u(r)=0$ (no intermolecular interactions) what does B_{2V} equal?



“From principle $u(r)$ can be calculated from quantum mechanics, but this is a difficult computational problem.” McQuarrie and Simon, pg.

$$u(r) \rightarrow -\frac{C_6}{r^6} \quad \text{Attraction potential}$$

$$u(r) \rightarrow \frac{C_{12}}{r^{12}} \quad \text{Repulsion potential}$$

The attraction potential is valid for large r , but the repulsion potential operates at large r .

Add them up:

$$u(r) = -\frac{C_6}{r^6} + \frac{C_{12}}{r^{12}}$$

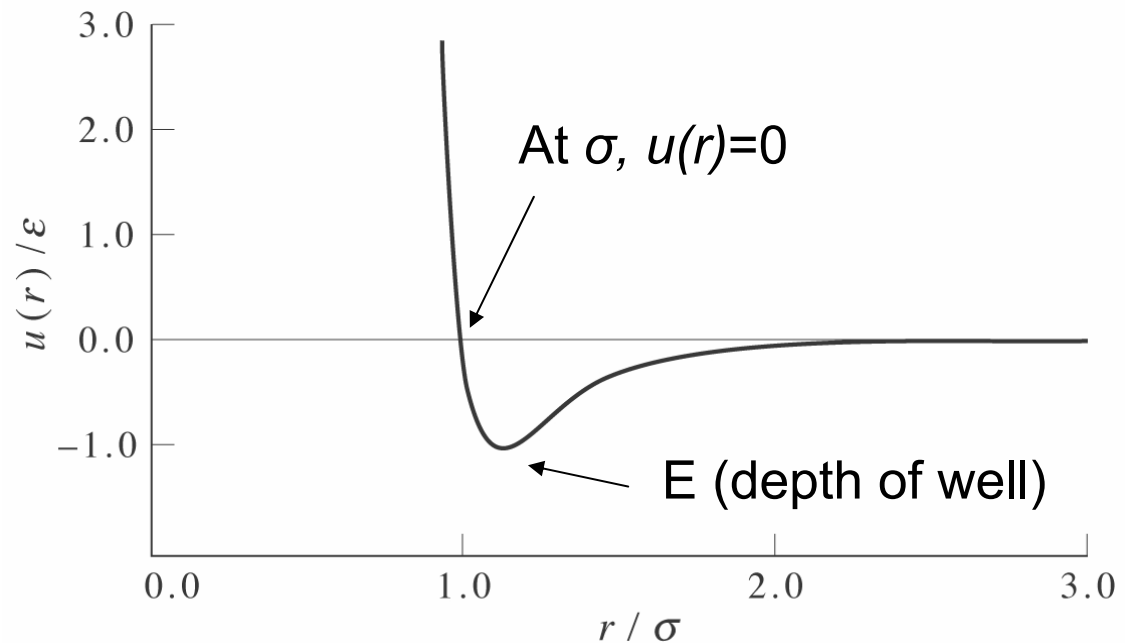




John Lennard-Jones

$$u(r) = 4\epsilon \left[\left(\frac{\sigma}{r} \right)^{12} - \left(\frac{\sigma}{r} \right)^6 \right]$$

$$c_{12} = 4\epsilon\sigma^{12} \quad c_6 = 4\epsilon\sigma^6$$



L-J parameters are used to calculate fluid properties such as viscosity, thermal conductivity, heats of vaporization, and crystal properties.



TABLE 2.7 (Table 16.7)

Lennard-Jones parameters, ϵ and σ , for various substances.

Species	$(\epsilon/k_B)/K$	σ/pm	$(2\pi\sigma^3 N_A/3)/\text{cm}^3 \cdot \text{mol}^{-1}$
He	10.22	256	21.2
Ne	35.6	275	26.2
Ar	120	341	50.0
Kr	164	383	70.9
Xe	229	406	86.9
H ₂	37.0	293	31.7
N ₂	95.1	370	63.9
O ₂	118	358	57.9
CO	100	376	67.0
CO ₂	189	449	114.2
CF ₄	152	470	131.0
CH ₄	149	378	68.1
C ₂ H ₄	199	452	116.5
C ₂ H ₆	243	395	77.7
C ₃ H ₈	242	564	226.3
C(CH ₃) ₄	232	744	519.4

ϵ is an energy

σ is a length

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How does B_{2V} relate to ε and σ ?

$$B_{2V}(T) = -2\pi N_A \int_0^{\infty} \left[\exp \left\{ -\frac{4\varepsilon}{k_B T} \left[\left(\frac{\sigma}{r} \right)^{12} - \left(\frac{\sigma}{r} \right)^6 \right] \right\} - 1 \right] r^2 dr$$

Substitute:

$$x = r / \sigma \quad \text{and} \quad T^* = k_B T / \varepsilon$$

$$B_{2V}(T^*) = -2\pi\sigma^3 N_A \int_0^{\infty} \left[\exp \left\{ -\frac{4}{T^*} \left[(x)^{-12} - (x)^{-6} \right] \right\} - 1 \right] x^2 dx$$

$$\text{Substitute: } B_{2V}^*(T^*) = \frac{B_{2V}(T^*)}{\frac{2}{3}\pi\sigma^3 N_A}$$

$$B_{2V}^*(T^*) = -3 \int_0^{\infty} \left[\exp \left\{ -\frac{4}{T^*} \left[(x)^{-12} - (x)^{-6} \right] \right\} - 1 \right] x^2 dx$$

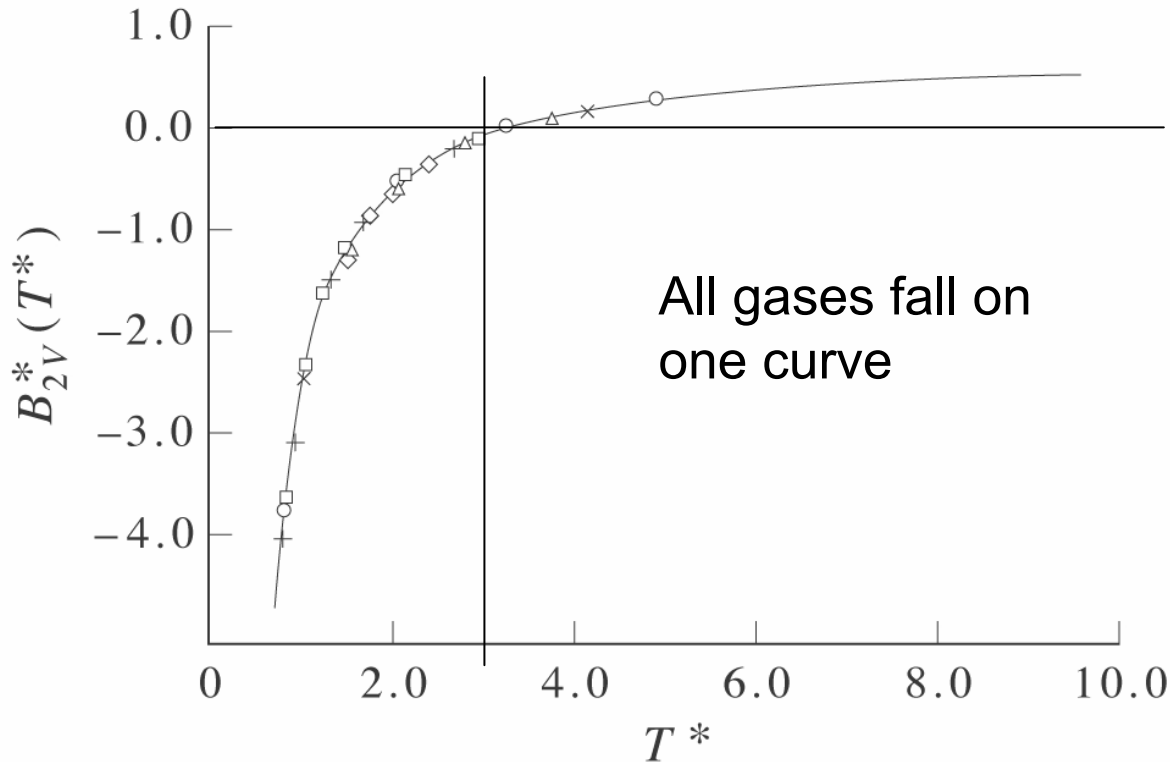
This expression needs to be evaluated numerically; luckily, tables of $B_{2V}^*(T^*)$ vs T^* are available.



Another LOCS Example

GAS-22

Plotting $B_{2V}^*(T^*)$ vs. T^* yields another example of law of corresponding states



Note: Typically, L-J parameters are determined from experimental B_{2V} values.

At $T^* \sim 3.2$, $B_{2V}(T^*) = 0$

How does a gas act at this temperature (called the Boyle temperature)?



Under conditions where we can ignore terms in P^2 and higher...

$$Z = \frac{P\bar{V}}{RT} = 1 + \frac{B_{2V}(T)}{RT} P$$

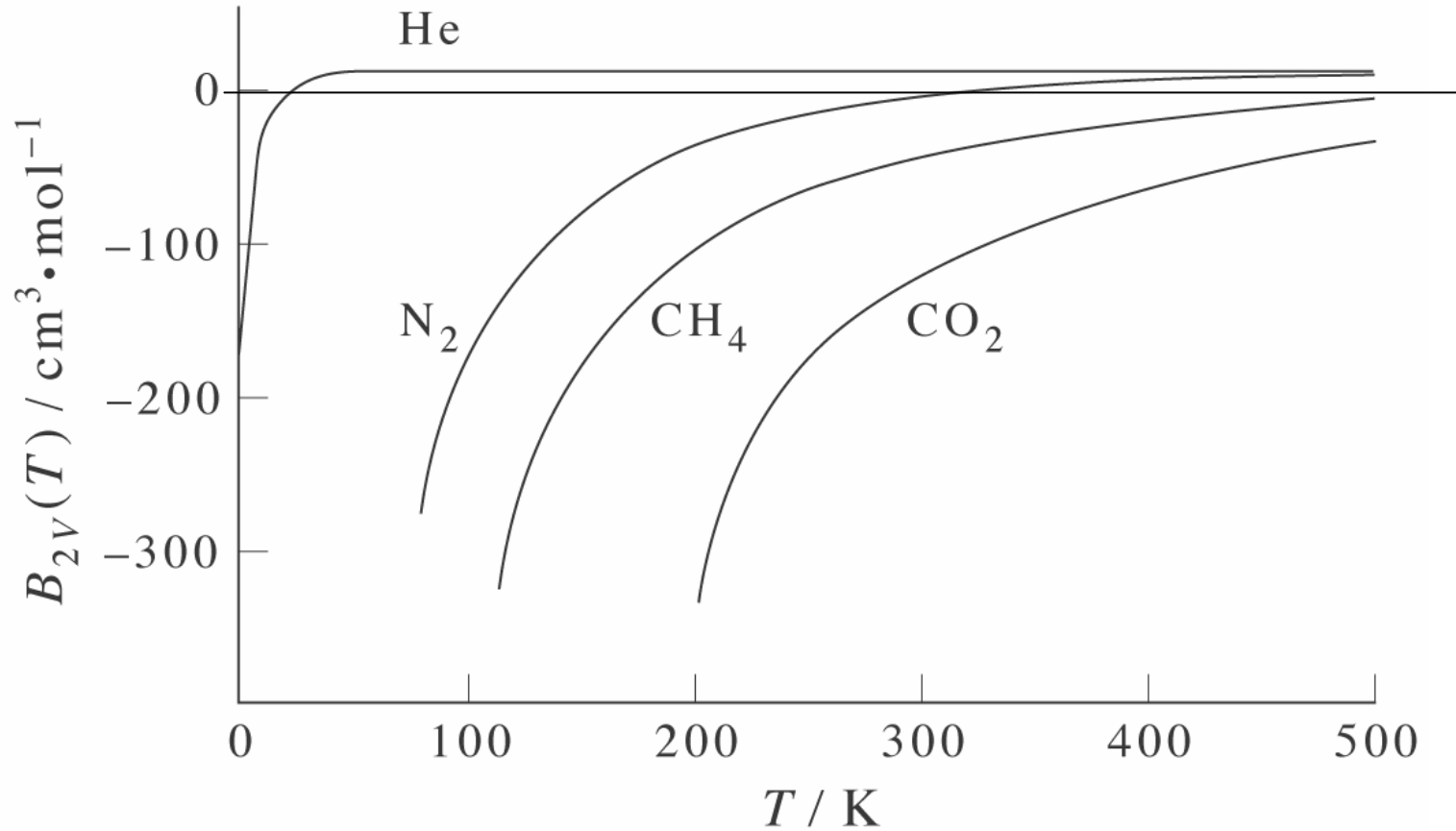
Multiply by RT/P and let $\bar{V}_{ideal} = \frac{RT}{P}$...

$$\bar{V} = \bar{V}_{ideal} + B_{2V}(T)$$

$$B_{2V}(T) = \bar{V} - \bar{V}_{ideal}$$

B_{2V} is the difference between the actual value of the molar volume and the ideal gas value!





$$B_{2V}(T) = \bar{V} - \bar{V}_{ideal}$$

Why do these plots look this way?



Understanding Attraction

GAS-25

The repulsive term of the L-J potential (the r^{-12} term) is not quite fully understood, but the r^{-6} attraction term is understood...

Dipole interactions

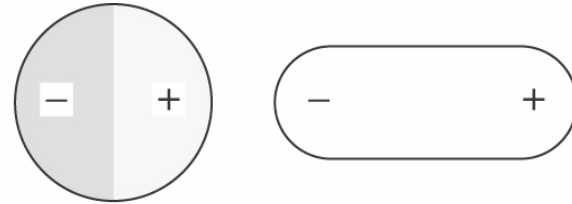


$$(a) \quad u_{d,d}(r) = -\frac{2\mu_1^2\mu_2^2}{(4\pi\epsilon_0)(3k_B T)} \frac{1}{r^6}$$



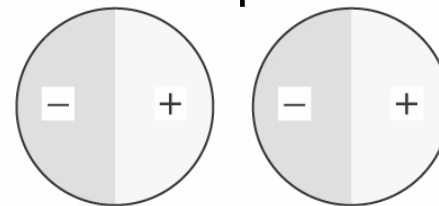
(b)

Induced Dipole-Dipole interactions



$$(c) \quad u_{induced}(r) = -\frac{\mu_1^2\alpha_2}{(4\pi\epsilon_0)r^6} - \frac{\mu_2^2\alpha_1}{(4\pi\epsilon_0)r^6}$$

Induced Dipole interactions

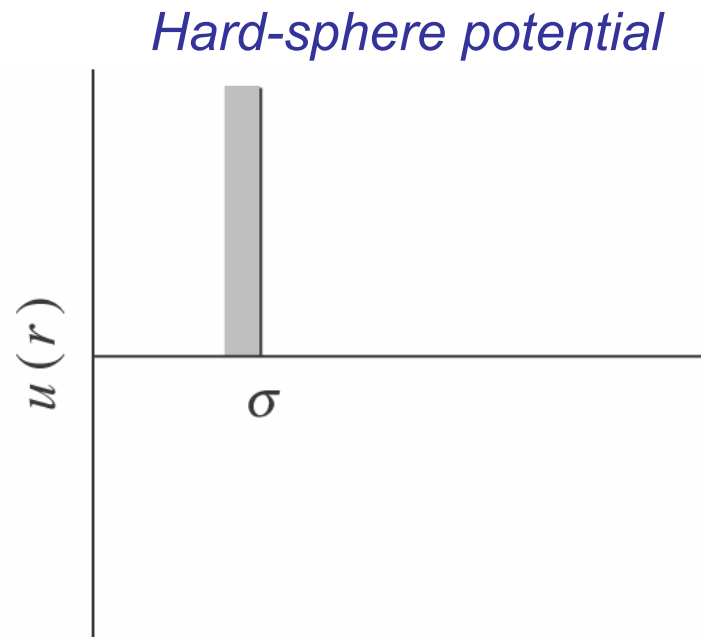


$$(d) \quad u_{disp}(r) = -\frac{3}{2} \left(\frac{I_1 I_2}{I_1 + I_2} \right) \frac{\alpha_1 \alpha_2}{(4\pi\epsilon_0)^2} \frac{1}{r^6}$$



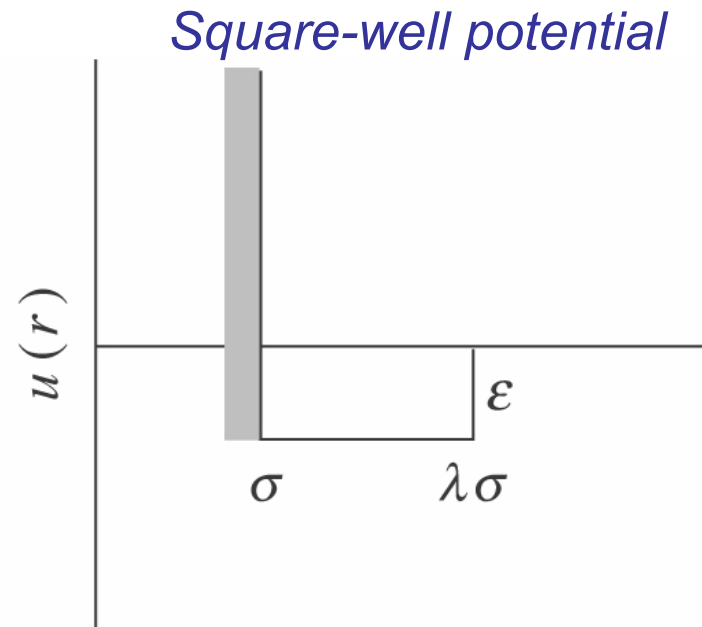
L-J is nice, but hard to use!

Isn't there an analytical solution for $u(r)$?
Yes, but we have to resort to simple models...



(a)

$$u(r < \sigma) = \infty$$
$$u(r > \sigma) = 0$$



(b)

$$u(r < \sigma) = \infty$$
$$u(\sigma < r < \lambda\sigma) = -\epsilon$$
$$u(r > \lambda\sigma) = 0$$



No attractive term! Good only at high T (with respect to ε/k_B).

$$\begin{aligned} B_{2V}(T) &= -2\pi N_A \int_0^{\infty} \left[e^{\frac{-u(r)}{k_B T}} - 1 \right] r^2 dr \\ &= -2\pi N_A \int_0^{\sigma} \left[e^{\infty} - 1 \right] r^2 dr - 2\pi N_A \int_{\sigma}^{\infty} \left[e^0 - 1 \right] r^2 dr \\ &= \frac{2\pi\sigma^3 N_A}{3} \end{aligned}$$

This expression is 4 times the volume of N_A spheres and σ can be thought of as the sphere diameter.

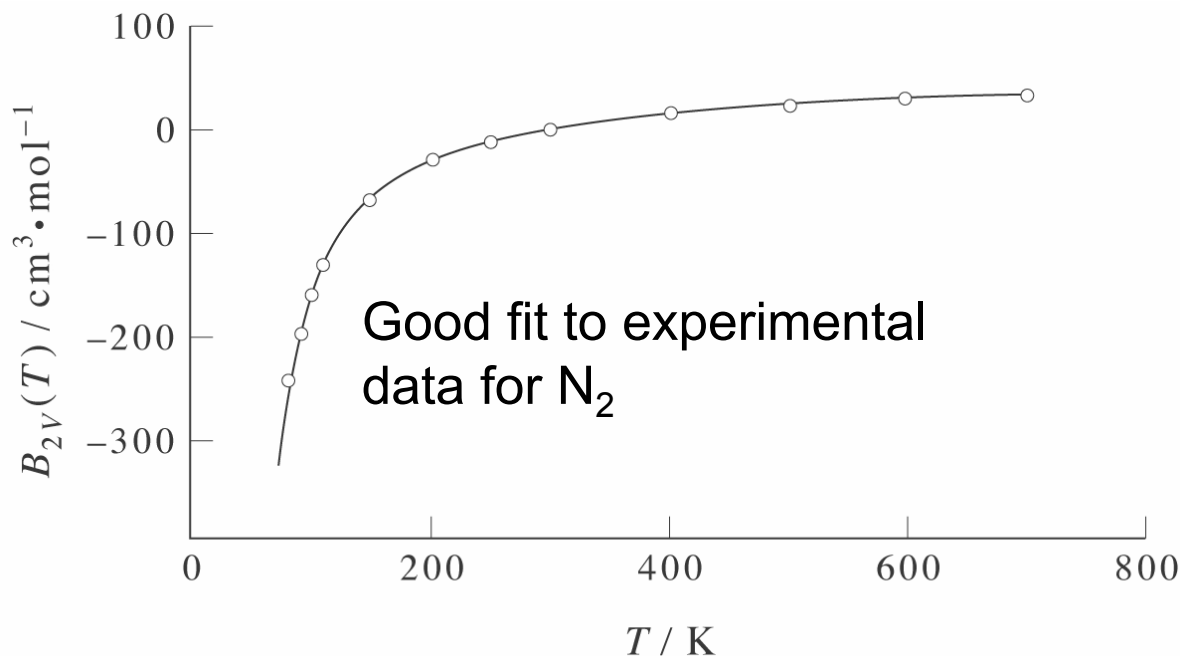
Independent of T , but remember... this expression is only valid for high T !



$$B_{2V}(T) = \frac{2\pi\sigma^3 N_A}{3} \left[1 - (\lambda^3 - 1) \left(e^{\varepsilon/k_B T} - 1 \right) \right]$$

What are the steps to get this answer?

What happens at $\lambda = 1$ or $\varepsilon = 0$?



	sqwm	L-J
σ (pm)	328	370
ε/k_B (K)	95.2	95.1
λ	1.58	N/A



1. Gases are rarely ideal ($PV=nRT$ fails miserably!).
2. van der Waals came up with an equation of state to account for non-idealities.
3. Cubic equations of state describe both the liquid and gaseous regions of the P-V isotherms.
4. At the critical point, VDW EOS has only one real root. Remember why this is important?!? (Hint: Think about a , b , and the critical values.)
5. The law of corresponding states says that all gases have the same properties if compared at corresponding conditions.



6. The virial expansion is in ways better than the VDW EOS.
7. The second virial coefficient is the most important and can be used to relate the properties of gases to molecular interactions.
8. Lennard-Jones came up with an expression for $u(r)$ in terms of the strength of molecular interactions (ϵ) and their size (σ).
9. LJ parameters come from experimental B_{2V} values.
10. London dispersion interactions can be understood through quantum mechanics.
11. Simple models (e.g., square well potential) can be used effectively to get molecular information about gases.

